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# INFLUENCE OF TEMPERATURE ON THE RETENTION BEHAVIOUR OF MEMBERS OF HOMOLOGOUS SERIES IN REVERSED-PHASE HIGH-PERFORMANCE LIQUID CHROMATOGRAPHY

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### SUMMARY

The capacity factors of  $C_6-C_{16}$  *n*-alkanols,  $C_6-C_{12}$  *n*-alkanal dinitrophenylhydrazones and  $C_6-C_{11}$  2-*n*-alkanone dinitrophenylhydrazones have been determined at various temperatures on MicroPak CH-10 and Nucleosil C-18 octadecyl reversedphase packings with aqueous methanol eluents. Linear log k' vs.  $C_m$ , log k' vs. 1/T,  $-\Delta H^0$  vs.  $C_m$  and log k' vs.  $-\Delta H^0$  relationships have been obtained. Equations are presented that describe the capacity factors as functions of both temperature and carbon number. The compensation temperatures determined according to Melander *et al.* indicate that the retention mechanisms underlying these reversed-phase separations are identical.

# INTRODUCTION

The awareness of the role of temperature in reversed-phase (RP) high -performance liquid chromatography (HPLC) has increased in recent years (see, e.g., Horváth and co-workers<sup>1,2</sup>, Colin *et al.*<sup>3</sup> and references cited therein). Melander *et al.*<sup>4</sup> applied the concept of enthalpy-entropy compensation to demonstrate the identity of the retention mechanism underlying RP separations in a few phase systems.

As by-products of systematic measurements in this Institute, a set of data relating to the influence of temperature on the retention behaviour of members of homologous series in several RP systems has been accumulated. It seems worthwhile presenting these measurements in an organized form as a contribution to the data base of the temperature dependence of retention in RP-HPLC.

# EXPERIMENTAL

Experiments were carried out with a liquid chromatograph assembled from a Model 6000 pump, a U6K injector, an M440 fixed-wavelength photometer, an R401 differential refractometer (Waters Assoc., Milford, MA, U.S.A.), an LC55 variablewavelength photometer (Perkin-Elmer, Norwalk, CT, U.S.A.) and an A-25 dualchannel recorder (Varian Aerograph, Walnut Creek, CA, U.S.A.). A commercial 25 cm  $\times \frac{1}{3}$  in. O.D. column (MicroPak CH-10, Varian Aerograph) and a custom-made 30 cm  $\times 1/4$  in. O.D. column slurry-packed with Nucleosil C<sub>18</sub> (Macherey, Nagel & Co., Bad Dürckheim, G.F.R.) were used. The columns were jacketed over their full lengths<sup>5</sup> and thermostated by a U10 circulating water-bath (MLW, Medingen, G.D.R.) Analytical-reagent grade methanol was obtained from Reanal (Budapest, Hungary).

The water content of the eluents filtered through GF/A and GF/D glass-fibre filters (Whatman, Clifton, NJ, U.S.A.) and vacuum degassed in an ultrasonic bath was determined daily (or after repeated degassing) from samples withdrawn from the inlet manifold of the pump. Water determinations were carried out in triplicate by Karl Fischer titration, with dead-stop end-point indication.

Samples were either analytical-reagent grade chemicals obtained from Merck (Darmstadt, G.F.R.), Fluka (Buchs, Switzerland), Condea (Hamburg, G.F.R.), BDH (Poole, Great Britain), Aldrich Europe (Beerse, Belgium) and Reanal (Budapest, Hungary), or synthesized, purified and analysed as described elsewhere<sup>6</sup>.

Retention times were determined from the distance of the peaks from the point of injection on the chromatograms.

# RESULTS

The retention of primary  $C_6$ - $C_{16}$  *n*-alkanols on a MicroPak CH-10 column was investigated<sup>7</sup>. Aqueous methanol (78.24%) was used as the eluent.  $t_0$  was determined by injecting a sufficient amount of 85% methanol to cause a noticable baseline disturbance. The capacity factors determined in the temperature range 30-60°C are given in Table I. The values are averages from five replicate determinations. The average reproducibility was better than 1% (relative).

# TABLE I

disturbance on the baseline.
(78.24%). to was determined by injecting the minimum amount of 85% methanol to cause a noticable
Column: Micropak CH-10 (Varian Aerograph), 25 cm × 1/8 in. O.D. Eluent: aqueous methanol
CAPACITY FACTORS (k') OF PRIMARY <i>n</i> -ALKANOLS AT VARIOUS TEMPERATURES

Chain carbon number, C <sub>a</sub>	Tempera	ature (°C)				
	30	35	40	45	50	60
	1/T · 103	(°K-1)				
	3.30	3.25	3.19	3.14	3.10	3.00
6	0.91	0.87	0.78	0.74	0.72	0.61
7	1.47	1.34	1.26	1.15	1.07	0.95
8	2.29	2.14	1.89	1.75	1.64	1.36
9	3.54	3.18	2.90	2.60	2.39	2.02
10	5.53	5.05	4.28	3.91	3.58	2.88
11	8.43	7.59	6.41	5.75	5.31	4.13
12	12.91	10.94	9.62	8.38	7.46	5.99
13	19.9	17.5	14.2	12.59	11.53	8.28
14	31.2	26.2	22.4	18.9	16.3	12.50
15	48.8	41.9	33.4	28.8	26	17.6
16	74.3	61.2	51.9	42.5	36	26.6

In connection with a study<sup>6</sup> of the retention behaviour of various saturated and unsaturated aldehyde and 2-*n*-alkanone dinitrophenylhydrazones (DNPHs), the temperature dependence of their capacity factors was also investigated. These separations were effected on a Nucleosil C<sub>18</sub> column. Again, aqueous methanol (80.0%) was used as the eluent.  $t_0$  was determined by injecting a sufficient amount of 68% methanol to cause a noticable baseline disturbance. The capacity factors of the C<sub>6</sub>-C<sub>12</sub> *n*-alkanal and 2-*n*-alkanone DNPHs are given in Table II. The values are averages from nine replicate determinations. The reproducibility was generally better than 0.8% (relative).

# TABLE II

# CAPACITY FACTORS (k') OF *n*-ALKANAL AND 2-*n*-ALKANONE DNPHs AT VARIOUS TEMPERATURES

Column: Nucleosil C<sub>15</sub> (Macherey, Nagel & Co.), 30 cm  $\times$  1/4 in. O.D. Eluent: aqueous methanol (80%).  $t_0$  was determined by injecting the minimum amount of 68% methanol to cause a noticable disturbance on the baseline.

Compound type	Chain	Temper	ature (°C)				
	carbon number,	20	30	40	43.6	50	60
	C.	1/T · 103	(°K-1)				
		3.41	3.30	3.19	3.16	3.10	3.00
n-Alkanal DNPHs	6	6.05	4.80	3.78	3.65	3.10	2.57
	7	8.91	6.95	5.38	5.14	4.30	3.51
	8	13.31	10.19	7.72	7.31	6.04	4.85
	9	20.0	16.9	11.32	10.60	8.55	6.67
	10	30.2	22.2	16.0	15.9	12.04	9.27
	12	70	48.8	33.7	30.7	24.2	17.8
2-n-Alkanone DNPHs	6	6.41	5.12	3.98	3.88	3.26	2.73
	7	9.39	7.36	5.62	5.43	4.53	3.72
	8	13.94	10.70	8.04	7.70	6.36	5.12
	11	48.2	34.7	24.3	22.7	1.80	13.59

### DISCUSSION

A number of conclusions can be drawn from the data in Tables I and II. It is known that an approximately linear relationship exists between  $\log k'$  and the carbon number of members of a homologous series:

$$\log k' = \log k'_a + aC_a \tag{1}$$

The intercepts, slopes and correlation coefficients  $(r^2)$  for *n*-alkanols and *n*-alkanal and 2-*n*-alkanone DNPHs at different temperatures are given in Table III. It can be seen that the fit is very good.

Another linear relationship exists at a particular carbon number between  $\log k'$ , and the reciprocal of the absolute temperature of the separation (van 't Hoff plots):

$$\log k' = \log k_{\rm T} + \frac{b}{T} \tag{2}$$

Temperature	1/T-103	n-Alkanols			n-Alkanal	DNPHs		2-n-Alkanon	te DNPHs	
()	(- <b>Y</b> _)	Intercept	Slope	<b>در</b>	Intercept	Slope	٩	Intercept	Slope	r
20	3.41	1	1	1	-0.2894	0.1773	7666'0	-0.2556	0.1759	1666.0
30	3.30	-1.1662	0.1901	0.9999	-0.3312	0.1689	0/66.0	-0.2981	0.1668	1666.0
35	3.25	-1.1583	0.1846	0.9997	ł	1	1	ł	I	1
40	3.19	-1.1677	0.1797	0.9997	-0.3772	0.1586	9666'0	-0.3512	0.1577	8666'0
43.6	3.16	I	I	I	-0.3684	0.1544	0.9999	-0.3502	0.1540	86660
45	3,14	-1.1617	0.1744	0.9998	١	۱	1	ł	۱	1
50	3.10	-1.1543	0.1700	0.9996	-0.40901	0.1491	0.9998	-0.3824	0.1487	8666'0
8	3.00	-1.1650	0.1614	<b>3666.0</b>	-0.4353	0.1403	6666'0	-0.4049	0.1397	6666'0

PARAMETERS OF LOG  $k' = LOG k_n + aC_n$  RELATIONSHIPS FOR THE THREE COMPOUND CLASSES AT VARIOUS TEMPERATURES

TABLE III

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The intercepts, slopes and correlation coefficients  $(r^2)$  for *n*-alkanols and *n*-alkanal and 2-*n*-alkanone DNPHs are given in Table IV. It can be seen that the fit is excellent.

The standard enthalpy of the transfer of a sample component from the mobile to the stationary phase can be calculated from the slope of the  $\log k' vs$ . 1/T relationship as

$$slope = \frac{-\Delta H^0}{2.3R}$$
(3)

The  $-\Delta H^{\circ}$  values thus calculated are given in Table IV. It can be seen that the  $-\Delta H^{\circ}$  values increase regularly with increasing carbon number. Therefore, another series of linear relationships can be derived:

$$-\Delta H^{0} = -\Delta H^{0}_{a} - cC_{a} \tag{4}$$

The slopes and intercepts are given in Table V. The slope can be considered as the methylene group increment of  $-\Delta H^0$ . This increment increases in the order *n*alkanol < *n*-alkanal DNPH < 2-*n*-alkanone DNPH, which agrees with the retention order. The intercepts represent the magnitude of  $-\Delta H^0$  associated with the transfer of the functional group alone. The intercepts increase in the order 2-*n*-alkanone DNPH < *n*-alkanal DNPH < *n*-alkanol, indicating that the mobile phase prefers a hydroxyl group to the aldehyde DNPH group, and the latter to the ketone DNPH functional group.

It can be also seen in Table II that both the intercept and the slope change regularly with the carbon number for all the three compound classes, *i.e.*, two linear equations can be fitted to the data: for the intercepts

$$\log k_T = d + \epsilon C_n \tag{5}$$

and for the slopes

$$b = f + gC_{\pi} \tag{6}$$

The parameters of eqns. 5 and 6 are given in Table V. Eqns. 5 and 6 combined with eqn. 2 result in a relationship that describes retention as a function of both temperature and carbon number:

$$\log k' = d + eC_a + \frac{f}{T} + g \cdot \frac{C_a}{T}$$
(7)

After substitution, these equations describing the capacity factors are as follows:

(a) for the *n*-alkanols:

$$\log k' = -1.09 - 0.128 C_{\pi} - \frac{22}{T} + \frac{96.5}{T} \cdot C_{\pi}$$
(8)

(b) for the *n*-aldehyde DNPHs:

$$\log k' = -1.52 - 0.134 C_{z} + \frac{359}{T} + \frac{92}{T} \cdot C_{z}$$
(9)

(c) for the 2-n-alkanone DNPHs:

$$\log k' = -1.52 - 0.124 \,\mathrm{C}_{\mathrm{g}} + \frac{370}{T} + \frac{88}{T} \cdot \mathrm{C}_{\mathrm{g}} \tag{10}$$

It-Alkanal DNPHs         2-n-Alkanone DNPL           Intercept         Slope         r <sup>1</sup> Intercept         Slope           9941         -1.64         0.419         0.9886         -1.69         0.4           9662         -1.5168         0.1345         0.9520         -1.5189         -0.1           9941         359         91.7         0.9886         370         88
9941         -1.64         0.419         0.9886         -1.69         0.41           9662         -1.5168         0.1345         0.9520         -1.5189         -0.15           9941         359         91.7         0.9886         370         88

Gy. VIGH, Z. VARGA-PUCHONY.

Vo.         variable         Intercept         Slope $r^2$ Intercept         Slope $r^3$ Intercept $-\Delta H^0$ 0.10 $-0.441$ 0.9941 $-1.64$ 0.419         0.9886 $-1.69$ $Log  K_1$ $-1.0920$ $-0.1285$ 0.9662 $-1.5168$ 0.1345         0.9520 $-1.5189$ $b$ $-22$ 96.5         0.9941         359         91.7         0.9886         370	iquation	Dependent	n-Alkanols			n-Alkanal	SHPHS		2-n-Alkano	ne DNPHs	
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	<i>.</i> 0	variable	Intercept	Slope	73	Intercept	Slope	~~~	Intercept	Slope	4
Log k <sup>7</sup> -1.0920 -0.1285 0.9662 -1.5168 0.1345 0.9520 -1.5189 b -22 96.5 0.9941 359 91.7 0.9886 370		0H0-	0.10	-0,441	0.9941	-1.64	0.419	0,9886	-1.69	0.402	0.95
b –22 96.5 0.9941 359 91.7 0.9886 370		Log k <sub>1</sub>		-0.1285	0.9662	-1.5168	0.1345	0.9520	-1.5189	-0.1236	0.92
		q	-22	96.5	0.9941	359	91.7	0,9886	370	88	56.0

Almost identical coefficients are obtained when the intercepts and slopes in Table III are fitted as functions of l/T.

Eqns. 8-10 can be used to determine the selectivity of the separation of two successive members of a homologous series, the so-called methylene group selectivity,  $\alpha_{n+1/n}$ . The expressions are as follows:

(a) for the *n*-alkanols:

$$\log a_{\pi+1/\pi} = -0.128 + \frac{96}{T} \tag{11}$$

(b) for the n-alkanal DNPHs:

$$\log a_{n+1/n} = -0.134 + \frac{92}{T} \tag{12}$$

(c) for the 2-n-alkanone DNPHs:

$$\log \alpha_{n+1/n} = -0.124 + \frac{88}{T} \tag{13}$$

The methylene group selectivities are generally similar. However, there is a subtle trend: the *n*-alkanols show the highest group selectivity, followed by the *n*-alkanal DNPHs and the 2-*n*-alkanone DNPHs. This order is opposite to the retention order. It seems that the lower the retention at a given carbon number (the more hydrophilic is the molecule), the higher is the effect of the addition of a methylene group on the retention.

Melander et al.<sup>4</sup> applied the principle of enthalpy-entropy compensation to the retention data observed in reversed-phase systems to test the identity of the retention mechanisms underlying the separations effected on different columns with different eluents. They derived the equation

$$\log \dot{k_T} = -\frac{\Delta H^0}{2.3R} \left(\frac{1}{T} - \frac{1}{\beta}\right) - \frac{\Delta G_{\rm B}}{2.3R\beta} + \log \varphi \tag{14}$$

where

 $k'_T$  is the capacity factor of the sample component at temperature T;

 $\beta$  is the compensation temperature;

- $\Delta H^{\circ}$  is the standard enthalpy of transfer of the sample component from the mobile to the stationary phase;
- $\Delta S^{\circ}$  is the associated change in standard entropy;

 $\Delta G_{\rm B}$  is the change of Gibbs' free energy; and

 $\varphi$  is the phase ratio of the column.

If a linear relationship can be observed between log k' determined at the harmonic average temperature,  $T_{\text{tarm}}$ , or close to the harmonic average temperature,  $T_{\text{eval}}$  and the  $-\Delta H^0$  values determined as described previously, then the entropyenthalpy compensation is indeed operative and the compensation temperature,  $\beta$ , can be evaluated from the slope of the log k' vs.  $-\Delta H^0$  relationship:

$$\log k' = \log k'_0 + \frac{1}{2.3R} \left( \frac{1}{T_{\text{eval}}} - \frac{1}{\beta} \right) (-\Delta H^0)$$
(15)

The harmonic average temperature,  $T_{harm}$  and  $T_{eval}$ , the actual evaluation temperature at which log k' values were taken, the parameters of eqn. 15, the intercept expressed as ln  $k'_0$  (to allow for direct comparison with the data in ref. 4) and the compensation temperature,  $\beta$ , are given in Table VI for the three compound classes. The extreme limits of ln  $k'_0$  and  $\beta$  determined by Melander *et al.*<sup>4</sup> are also given.

### TABLE VI

COMPENSATION TEMPERATURE AND RELATED DATA FOR THE THREE COMPOUND CLAS-SES

Compound type	Tharm	Teval	Log k' vs.	g k' vs. $-\Delta H^\circ$ relationships			Compensation
	(°K) (°K	(°K)	Intercept	Slope	r²	•	temperature, β (°K)
n-Alkanols	316	318	-1.11	0,3932372	0.9936	-2.56	743
n-Alkanal DNPHs	317	317	-0.963	0.3674046	0.9844	-2.22	676
2-n-Alkanone DNPHs	317	317	-0.984	0.3822803	0.9986	-2.27	709
Melander et al.4	- <u> </u>	313		·	0.965	2.97	647
						-2.17	596
	<u></u>					-3.13	639

The high  $r^2$  values indicate that the compensation mechanism is indeed operative in each instance. Both the intercepts and the compensation temperatures are within the ranges determined by Melander *et al.*<sup>4</sup>. This means that although the sample components, the eluents and the stationary phases were different (octadecylsilicas with both bulk and brush-type bonded phases) in the two studies the mechanism underlying the separations was identical.

### CONCLUSIONS

The data set obtained from studies on the reversed-phase retention behaviour of *n*-alkanols and *n*-alkanal and 2-*n*-alkanone DNPHs at different temperatures was analysed. The separations were carried out on octadecylsilica columns with both bulk and brush-type bonded phases, using aqueous methanol solutions as eluents. In all instances linear relationships were found between log k' and C<sub>n</sub>, log k' and l/T,  $-\Delta H^0$  and C<sub>n</sub> and log k' and  $-\Delta H^0$ . Equations describing log k' as function of both temperature and carbon number were obtained. Entropy-enthalpy compensation behaviour could be observed with all three compound classes. The compensation temperatures are similar to those obtained by Melander *et al.* for other octadecylsilica packings<sup>4</sup> with buffered aqueous acetonitrile eluents and very polar sample components, indicating that the underlying separation mechanisms are identical.

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8

### NOTE

Since the completion of this manuscript, another paper dealing with enthalphyentropy compensation was published by Melander *et al.*<sup>3</sup>. It was concluded that there is a linear relationship between the log k' and both the eluent composition and the reciprocal of the absolute temperature (eqn. 12a and Table I in ref. 8). For *n*-alkylbenzenes in an acetonitrile-water/Partisil ODS-2 system linear relationships were observed between the parameters of eqn. 12a in ref. 8 and the alkyl carbon number. By selecting a constant eluent composition,  $\varphi$ , as in this paper, and substituting for  $A_1$ ,  $A_2$  and  $A_3$ , the parameters of eqn. 12a in ref. 8, the observed linear relationship, one arrives at an equation equivalent to eqn. 7 in this paper. This also means that eqn. 12a (or 12b) in ref. 8 can be extended to include the carbon number as a third variable, resulting in an equation containing all of the primary parameters that influence the magnitude of retention in RP chromatographic systems. Although it would be instructive, one cannot check our data against eqn. 7 in ref. 8 because the dependence of k' on the solvent composition is not reflected by these data.

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